

FUEL CELL HUMIDIFYING SYSTEM

BACKGROUND OF THE INVENTION

Field of the Invention

The present invention relates to a fuel cell humidifying system having a water permeable humidifier, and relates in particular to a technology for preventing freezing of humidifier and resulting clogging of the fuel cell.

Description of the Related Art

A fuel cell that uses a solid polymer membrane for the electrolyte membrane, for example, is comprised by stacking a plurality of unit cells.

A unit cell is comprised by a core of a solid polymer membrane of ionic conductivity in intimate contact with a fuel-electrode (anode) and an air-electrode (cathode) on each surfaces thereof. When hydrogen gas is supplied through the fuel gas passage formed as an U-shaped groove on the surface facing the fuel-electrode and air is supplied simultaneously through the oxidizer passage formed as an U-shaped groove on the surface facing the air-electrode, electricity is generated as a result of electrochemical reaction between the electrodes in each unit cell.

To maintain high electrical generation efficiency, the solid polymer membrane must be maintained in a water-saturated state so as to enable the solid polymer to function as a proton (hydrogen ions) conductive electrolyte.

However, during the electricity generation process, the solid polymer membrane is sometimes subjected to conditions that promote drying, due to various factors including the fact that the water generated by chemical reaction is transported out of the system. Therefore, to maintain good ionic conductivity, it is necessary to supply moisture to the solid polymer membrane.

For this reason, a conventional approach is to devise a humidifying system to humidify dry gases such as the air to be supplied to the air-electrode side and the hydrogen to be supplied to the fuel-electrode side by passing both gases through a water permeable humidifier so as to obtain wet gases for humidifying the solid polymer membrane.

Here, the term "dry gas (es)" means the gas has a relative low humidity, such as the gas contains little moisture or contains moisture insufficient to humidify the solid polymer membrane, and the term "wet gas (es)" means the gas has a relative high humidity, such as the gas contains moisture sufficient to humidify the solid polymer membrane

This type of humidifier is provided with a hollow threaded membrane to permit water to infiltrate in the direction of the film thickness (refer to Japanese Patent Application, First Publication, No. Hei 7-71795, and Japanese Patent Application, First Publication, No. Hei 8-273687), and for example, humidification of the air-electrode side is carried out as follows.

That is, while dry air is being forced through a jacket containing a packing comprised by an assembly of hollow thread membranes using a charging apparatus such as a supercharger, wet out-gas discharged from the air-electrode side is forced through the hollow section inside the hollow thread membrane so that the moisture contained in the wet out-gas can infiltrate through the porous surface of the hollow thread membrane and disperse on the outside of the hollow thread membrane as water vapor to add humidity to the dry air flowing through the inter-thread spaces formed by the thread membranes.

However, in the fuel cell humidifying system provided with a water permeable humidifier, water is produced by the redox reaction of oxygen and hydrogen, and the produced water is recovered from the wet out-gas and transferred to the dry gas through the hollow thread membrane in the humidifier, and is reused to add humidity to the fuel cell. Therefore, during the cold spell or in cold climate, it is unavoidable to subject the moisture in the humidifier to freezing conditions.

Freezing creates problems in the following manner. Because the pore diameter of the hollow thread membrane is extremely fine (4 nm) and can exert a very high surface tension force, the moisture condensed in the pores is subjected to supercooling and does not undergo phase transformation (water to ice) but, because the internal diameter of the hollow section of the hollow thread membrane is relatively large (0.37 mm) and is not subjected to supercooling, the moisture becomes frozen.

When the moisture becomes frozen in the interior of the hollow thread membrane, it becomes difficult to operate the system at its optimal capacity.

Also, it is also possible that, if dust particles and the like having diameters larger than the inside diameters of the hollow section or the pores of the membrane are mixed in the wet out-gas from the fuel cell, such particles may block the entrance to the hollow section or plug up the pores of the membrane to cause a pressure increase at the entrance to the hollow thread membrane or decrease in the recoverable amount (percent) of water, resulting in degradation in the performance of the inherent capability of the fuel cell humidifying system.

Similarly, for the dry gas supplied by the supercharger and the like through the gas passage may also be subjected to detrimental effects of freezing and clogging.

Accordingly, when freezing or clogging is generated in the hollow thread membrane of the humidifier, it becomes difficult to operate the fuel cell at its inherent optimal capability by continuing to recover a sufficient amount of water from the wet out-gas to resupply an appropriate degree of humidity to the fuel cell.

SUMMARY OF THE INVENTION

The present invention is provided in view of the background information described above, and it is an object of the present invention to provide a technology for preventing freezing and clogging in the humidifier.

To resolve the problem described above, the present invention provides the following structure of the fuel cell humidifying system.

That is, the fuel cell humidifying system of the present invention is for providing a dry gas (in the embodied case, dry air Ad) and an exhaust gas (in the embodied case, wet out-air OAw) discharged from the fuel cell (1) into a water permeable type humidifier (3) so as to recover moisture contained in the exhaust gas in the dry gas to produce a wet gas (in the embodied case, wet air Aw) which is supplied to the fuel cell; and the system has a flow path switching mechanism (in the first embodiment, this mechanism comprises a first three-way valve 4, a second three-way valve 5, a flow adjusting valve 6, sweep piping 9, and a control apparatus; and in the second embodiment, this mechanism comprises first reverse cleansing piping 31, second reverse cleansing piping 32, first exhaust piping 33, second exhaust piping 34, a pressure sensor 35, a first shutoff valve 41, a second shutoff valve 42, a third shutoff valve 43, a fourth shutoff valve 44, a fifth shutoff valve 45, a sixth shutoff valve 46, a seventh shutoff valve 47, and a control apparatus) for switching gas passages (in the embodied case, air piping 7, out-air piping 8) leading to the humidifier.

According to the fuel cell humidifying system, clogging in the humidifier can be prevented by switching the flow direction in the humidifier.

In this case, the flow path switching mechanism may adopt a mechanism for flowing a dry gas in the exhaust gas passage in the humidifier (in the embodied case, the wet out-air passage) or a mechanism for reversing the flow direction of exhaust gas in the humidifier.

In the former flow path switching mechanism, by flowing the dry gas in the exhaust gas passage in the humidifier before the moisture freezes, water vapor that causes freezing can be swept out so that freezing can be prevented beforehand.

In the latter flow path switching mechanism, even if clogging are generated in the exhaust gas passage in the humidifier by dust particles and other such substances

contained in the exhaust gas flowing in the forward direction, because the exhaust gas flow direction can be reversed, such clogging can be eliminated by reverse flow cleansing.

BRIEF DESCRIPTION OF THE DRAWINGS

Fig. 1 is a schematic diagram of the gas flow during the normal mode of operation in the fuel cell humidifying system in a first embodiment.

Fig. 2 is a schematic diagram of the gas flow during the gas sweeping mode of operation in the fuel cell humidifying system in the first embodiment.

Fig. 3 is a schematic diagram of the gas flow during the normal mode of operation in the fuel cell humidifying system in a second embodiment.

Fig. 4 is a schematic diagram of the gas flow during the reverse flow cleansing mode of operation in the fuel cell humidifying system in the second embodiment.

Fig. 5 is a schematic diagram of a third embodiment of the fuel cell humidifying system.

DESCRIPTION OF THE PREFERRED EMBODIMENTS

A first embodiment will be presented in the following with reference to the drawings. The structural features of the fuel cell and the hollow thread membrane serving the function of a water permeable membrane in the present invention are the same as those described in the Description of the Related Art, and therefore, their explanations are omitted.

First Embodiment

Fig. 1 shows a schematic diagram of the configuration of a fuel cell humidifying system in the first embodiment in the normal mode of operation, and Fig. 2 shows the same in the gas sweeping mode of operation.

In these diagrams, the reference numeral 1 relates to a solid polymer electrolyte type fuel cell (fuel cell hereinbelow); 2 to a supercharger; 3 to a humidifier; 4 to a first three-way valve; 5 to a second three-way valve; 6 to a flow adjusting valve; 7 to an air piping; 8 to an out-air piping; and 9 to a sweep piping, and the system components including the above are controlled by a control apparatus which is not shown.

First, with reference to Fig. 1, the overall system configuration of the present fuel cell humidifying system and the operation of the system in the normal mode will be explained.

The air-electrode (cathode) of the fuel cell 1 is connected to the air piping 7 for

supplying outside air (referred to as dry air Ad) which is inhaled from an intake opening 11 and serving as the oxidizer, to an oxidizer inlet opening 12; and the out-air piping 8 for discharging the out-gas (referred to as wet out-air OAw hereinbelow) which flows from the oxidizer outlet opening 13, to an exhaust opening 14.

The supercharger 2, the humidifier 3, the first three-way valve 4 are provided in the air piping 7 from the upstream side to the downstream side of flowing dry air Ad (that is, from the intake opening 11 to the fuel cell 1) in the stated order.

The second three-way valve 5, the humidifier 3, and the pressure adjusting valve 16 are provided in the out-air piping 8 from the upstream side to the downstream side of flowing wet out-air OAw (that is, from the fuel cell 1 to the exhaust opening 14) in the stated order.

The sweep piping 9 branches off from the air piping 7 between the supercharger 2 and the humidifier 3, and bypasses the humidifier 3, the first three-way valve 4 and the fuel cell 1 and is connected to the second three-way valve 5. Furthermore, the flow adjusting valve 6 is provided with the sweep piping 9.

Also, a discharge piping 18 communicating with the exhaust opening 17 is connected to the first three-way valve 4 provided in the air piping 7.

During the normal mode of operation, the flow adjusting valve 6 is fully-closed, and the outside air (dry air Ad) inhaled from the intake opening 11 recovers moisture from the wet out-air OAw discharged from the fuel cell 1 in the humidifier 3, that straddles both air piping 7 and the out-air piping 8, to produce wet air Aw which is supplied to the fuel cell 1.

The wet air Aw is used for electrical generation together with the hydrogen supplied from a high pressure hydrogen tank (not shown) to the fuel cell 1 as well as for supplying moisture to maintain the solid polymer membrane in the fuel cell 1 in the water-saturated state.

On the other hand, the wet out-air OAw, that is used for humidifying the dry air Ad and is dehumidified, becomes dry out-air OAd and is discharged from the exhaust opening 14.

Next, the gas sweeping mode of operation of the fuel cell humidifying system is an example of the system operation, and will be explained with reference to Fig. 2. The gas sweeping mode is carried out while the fuel cell 1 is stopped and when the outer temperature detected by the temperature sensor (not shown) becomes equal to 0°C or below.

Prior to the gas sweeping mode, the flow adjusting valve 6 is changed from "close" to "open", and the first three-way valve 4 is controlled in such a way that the